# **Performance Evaluation of Sewage Treatment Plants in Ganga Front Towns (2019)**





## **Central Pollution Control Board**

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## **CONTRIBUTIONS**



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## <span id="page-6-0"></span>**CHAPTER 1: INTRODUCTION**

### <span id="page-6-1"></span>**1.1 Background**

In urban areas, water is tapped from rivers, streams, wells and lakes for domestic and industrial consumptions. Almost 80% of the water consumed for domestic use, comes back as wastewater. In most of the cases untreated wastewater is let out which either sinks into the ground as a potential long-term pollutant of ground water or is discharged into the natural drainage system causing pollution in downstream areas.

The water that emerges after household uses contains, organic materials from food, oils, detergents, dust and dirt from floor, soaps and oils and biological material from human body all these referred to as Grey Water. The water used to flush toilets to evacuate human excreta is called Black Water/ Sewage.

In terms of purification technology, grey water is easier to purify as compared to black water, i.e sewage. In India, both grey water and black water are generally mixed and flow to the inlet sump of sewage treatment plants through the sewerage network in the catchment area and is treated as "Raw Sewage" in the STP.

Chemically, wastewater is composed of organic and inorganic compounds. Organic components may consist of carbohydrates, proteins, fats, greases, surfactants, oils, pesticides, phenols, etc., Inorganic components may consist of heavy metals, nitrogen, phosphorus, sulfur, chlorides etc. The amount of oxygen required by micro-organisms for decomposing the organic matter present in sewage is called Biochemical Oxygen demand (BOD). The amount of oxygen needed to chemically oxidize both organic and inorganic matter present in the same sewage with is called as Chemical Oxygen demand (COD).

Raw sewage may have fecal contamination, which may cause serious problem due to their potential for causing diseases from pathogens (disease causing organisms). Coliforms come from the same sources as pathogenic organisms i.e. faeces of warm-blooded animals and humans. Coliforms are relatively easy to identify, are usually present in larger numbers than more dangerous pathogens, and respond to the environment, wastewater treatment, and water treatment similarly to many pathogens. **Hence, testing for coliform bacteria can be a reasonable indication of whether other pathogenic bacteria are present.** Coliform count is analyzed with reference to Total coliform (TC) and faecal coliform.

High concentration of total suspended solids (TSS) is also a major feature of raw sewage. The visible black colour of raw sewage is mainly because of this high TSS tagging it as black water. The raw

sewage may also have strong unpleasant smell caused due to septic condition and stagnancy resulting in hardship and health hazard.



**Figure 1: Composition of typical municipal wastewater**

S. no.	<b>Parameters</b>	Ranges
1	pH	7.15-7.65 unit
2	<b>BOD</b>	200-250 mg/1
3	COD	350-500 mg/1
4	Dissolved Solids	850-1350 mg/l
5	<b>Suspended Solids</b>	350-450 mg/l

<span id="page-7-1"></span><span id="page-7-0"></span>**Table 1 Physio-Chemical composition of typical municipal wastewater**

In present time, generation and management of all community sewage has become a major problem in densely populated urban areas and far-off rural areas. The generated sewage from the cities and human settlements has the potential of contaminating the surface water such as rivers, lakes and underground water bodies as well as causing serious health effects in human population in the areas living nearby the drains and contaminated rivers.



#### <span id="page-8-2"></span>**Figure 2: The overall structure of the water system of a metropolis**

#### <span id="page-8-0"></span>**1.2 Various Treatment technologies**

#### <span id="page-8-1"></span>**1.2.1 Sewage Treatment Methods**

Most of the technologies of Sewage Treatment treats the Wastewater in 3 phases:

- A. Pre-treatment Process
- B. Primary (Physical/Mechanical Solid removal)
- C. Secondary (Biological treatment/bacterial decomposition),
- D. Tertiary (Extra filtration& Disinfection)

*A. Pre-treatment* of sewage involves removal of all solid materials from the raw sewage before they damage or clog the pumps and objects commonly recovered include trash, tree limbs, leaves, branches, glasses, plastic materials and other large objects. This process may also include a sand or grit channel or chamber for the removal of grit or sand, where the velocity of the incoming sewage is adjusted to allow the settlement of sand and grit. Grit removal is necessary to (1) reduce formation of heavy deposits in aeration tanks, aerobic digesters, pipelines, channels, and conduits; (2) reduce the frequency of digester cleaning caused by excessive accumulations of grit; and (3) protect moving mechanical equipment from abrasion and accompanying abnormal wear. B. *Primary treatment* removes material that will either float or readily settle out by [gravity.](https://www.britannica.com/science/gravity-physics) It includes the "primary sedimentation tanks" or "primary [clarifiers"](https://en.wikipedia.org/wiki/Clarifier). The tanks are used to settle sludge while grease and oils rise to the surface and are skimmed off.

*C. Secondary Treatment* or Biological sewage treatment is a process where biological organisms are cultured and allowed to consume the organic matter and multiply their population. Biological organisms secrete enzymes through their cell walls which solubilize the organic matter and the solution is drawn back by organism as food and multiplies their number. The multiplied organisms are settled out and the clear treated sewage is almost free from the organic matter.

*D. Tertiary treatment* is not always necessary, but disinfection is an important step before discharge of treated sewage. Depending on the end-use of the effluent or for achieving stringent standards for discharge in water bodies, a post-treatment/tertiary filtration treatment step may be required to remove residual suspended solids and/or dissolved constituents followed by disinfection for removal of pathogens.

The biological metabolism can be by any of the following:

- A. Aerobic Digestion by organisms needing oxygen for growth
- B. Anaerobic Digestion by organisms that grow without oxygen
- C. Facultative process- Both aerobic and anaerobic system works as per Dissolved Oxygen (DO) level in the system.

#### **A. Aerobic Digestion**

The Aerobic system digestion for sewage treatment is carried out by aerobic bacteria which consumes the biodegradable carbonaceous and nitrogenous material and nutrient present in sewage in the presence of oxygen resulting in formation of secondary molecules which can be easily discharged into environment.



<span id="page-9-0"></span>**Figure 3: Diagrammatic representation of aerobic degradation of organic matter.** *Source: Dr. Akepati S. Reddy, Thapar Centre for Industrial Research & Development, Punjab*



<span id="page-10-0"></span>**Figure 4: Flow Diagram of Typical Aerobic Mechanized Biochemical Treatment System**

The most commonly used aerobic treatment systems are as follows:

**Activated Sludge Process (ASP)** – It consists of an aeration tank, where organic matter is stabilized by the action of consortium of bacteria (Mixed Liquor - MLSS) under aeration and a secondary sedimentation tank/clarifier (SST), where the biological cell mass is separated from the effluent of aeration tank and the settle sludge is recycled partly to the aeration tank and remaining is wasted and disposed of through sludge handling units.

The important parameters of ASP process are oxygen supply, mixing characteristics, F/M ratio and return activated sludge flow (RAS). BOD & COD reduction up to 95 % can be achieved using ASP. ASP system have many modifications & differ from each other in the manner in which the influent is applied, microorganisms are utilized, and hardware is assembled e.g. Tapered aeration, Extended aeration, Sequencing batch reactor (SBR), Mixed Bed Biofilm Reactor (MBBR) etc.

**Sequencing batch reactor (SBR)** – The SBR is a type of suspended growth aeration treatment system and consists of a single completely mixed reactor in which all the steps of the activated sludge process occur in batches. The reactor basin is filled within a short duration and then aerated for a certain period of time. After a settling phase the supernatant treated sewage is decanted and disinfected. This process is popular because entire process uses one reactor basin.

Enhanced Nitrogen (N) and Phosphorus (P) removal can be achieved in an SBR. P release and short chain volatile fatty acid (SCVFA) uptake occur during the anaerobic react (stir) operation after fill. P uptake, BOD reduction, and nitrification occur during the aerobic cycle. Denitrification is achieved during the anoxic stir and settling/decant cycles. BOD & COD reduction up to 95 % can be achieved using SBR technology. SBR system can be classified in two type based on feed flow i.e. Conventional SBR and continuous flow SBR.



<span id="page-11-0"></span>**Figure 5: ( A) Typical schematic representation of working principle. (B) Schematic representation of working principle of SBR**



<span id="page-11-1"></span>**Figure 6: A STP based on SBR technology at Tapovan, Rishikesh**

**Moving Bed Biofilm reactor (MBBR)** – MBBR process is a type of continuous flow attached growth aeration treatment system. This technology employs thousands of polyethylene biofilm carriers operating in mixed motion within an aerated wastewater treatment basin. Each individual biocarrier increases productivity through providing protected surface area to support the growth of heterotrophic and autotrophic bacteria within its cells.

MBBR system can be operated with and without sludge recirculation. MBBR process offer some advantages over conventional ASP like increased biomass, reduced volume requirement, lower HRT, high organic loading rate and enhanced nitrification/denitrification in one reactor etc. BOD& COD reduction 80-95 % can be achieved using MBBR technology



**Figure 7: Schematic representation of working principle of MBBR**

#### <span id="page-12-0"></span>**B. Anaerobic Digestion**

Anaerobic digestion is carried out by the organisms which do not require oxygen for metabolism and multiplication. Anaerobic digestion, as a unit process in municipal sewage treatment has been in use since the beginning of this century. Anaerobic treatment itself is very effective in removing of biodegradable organic pollutant leaving mineralised compounds like NH4+, PO4  $\frac{3}{2}$ , S  $\frac{3}{2}$  in the treated effluent. It is employed for stabilization of sludge solids from primary and secondary sedimentation tanks either in closed digesters or open lagoons. In general, the anaerobic biochemical reactions involve four successive stages, namely: (i) hydrolysis, (ii) acidogenesis, (iii) acetogenesis, and (iv) methanogenesis.



<span id="page-12-1"></span>**Figure 8: Diagrammatic representation of anaerobic degradation of organic matter**





#### <span id="page-13-0"></span>**Figure 9: Typical Anaerobic Treatment System Flow diagram**

The most commonly used anaerobic treatment systems are as follows:

**Up-flow Anaerobic Sludge Blanket** (UASB) is a type of suspended growth continuous flow anaerobic digestion system &most widely and successfully used high-rate anaerobic technology for treating several types of wastewater. UASB uses an anaerobic process whilst forming a blanket of granular sludge (size 1-3 mm) which suspends in the tank. Wastewater flows upwards through the blanket and the treatment process takes place by solids entrapment and organic matter conversion into biogas and sludge. The produced biogas bubbles automatically rise to the top of the reactor, carrying water and solid particles, i.e. biological sludge and residual solids. The gases produced cause internal recirculation and upward velocity which keep the granules in suspension.

The design of the UASB reactor combines the features of a high-rate bioreactor with those of an inbuilt secondary clarifier at the top. In UASB reactors the amount of anaerobic sludge generally is in the range 35-40 kg VSS/ $m<sup>3</sup>$  reactor volume (settler included). Wastewater having organic loading rate in the range of 5-20 kg COD/m3/day can be treated effectively using UASB with 80-95 %reduction in BOD& COD.



**Figure 10: Schematic representation of UASB**

#### <span id="page-14-0"></span>**C. Facultative Process**

Facultative treatment process uses both - aerobic and anaerobic processes of digestion in a single pond and occurs simultaneously. This is confined to stabilization ponds where the upper portion is aerobic and the settled sludge undergoes anaerobic process at the pond bottom.



**Figure 11: Diagrammatic representation of Facultative Process (CPHEEO, 2013)**

<span id="page-14-1"></span>The most commonly used facultative treatment system is as follows:

**Waste Stabilization Pond (WSP):** Waste or [wastewater](https://sswm.info/content/wastewater) **s**tabilization ponds (WSPs) are large, manmade water bodies in which black water, greywater or faecal sludge are treated by natural occurring processes and the influence of solar light, wind, microorganisms and algae . The ponds can be used individually, or linked in a series for improved treatment. There are three types of ponds, (1) anaerobic, (2) facultative and (3) aerobic (maturation), each with different treatment and design characteristics.

Major source of oxygen are natural reactions and  $O_2$  produce due to photosynthesis. WSPs are lowcost for O&M while BOD and pathogen removal is high. Major disadvantages include; large area, odour problem, insects and ground water contamination. BOD and COD reduction in the range of 50-90% can be achieved using WSP technology.



**Figure 12: Schematic representation of WSP**

#### <span id="page-15-2"></span><span id="page-15-0"></span>**1.3 Factors affecting efficiency of STPs**

<span id="page-15-1"></span>**1.3.1 Sludge retention time (SRT):** The sludge retention time (SRT) is the average time the activated-sludge solids are in the system. The SRT is an important design and control parameter for the activated-sludge process and is usually expressed in days. SRT of 3-4 days is generally considered good for the optimum functioning of a STP. Selection of sludge age is most fundamental & important decision in the design of activated sludge process. Treatment plant can be classified in three categories i.e. short sludge age (1-5 days), medium sludge age (10-15 days) and long sludge age (> 20 days)

<span id="page-16-1"></span>



<span id="page-16-0"></span>**1.3.2 Food to mass ratio:** The term **Food** to Microorganism **Ratio** (F/M) is actually a measurement of the amount of incoming **food** divided by the mass of Microorganisms in the aeration system. Ideal F: M ratio ranges from 0.1 to 0.6, for the optimum functioning of a STP.



**Figure 12: F/M ratio dynamics with respect to time**

<span id="page-17-0"></span>**1.3.3 Sludge volume index:** Sludge Volume Index (SVI) is an extremely useful operational parameter to measure in a wastewater treatment process. Sludge Volume Index (SVI) is used to describe the settling characteristics of sludge in the aeration tank in Activated Sludge Process. It is a process control parameter to determine the recycle rate of sludge. If SVI ranges between 100-150  $ml/g$  is considered to be ideal for the proper functioning of a STP. SVI is used as an empirical measure which links the sludge characteristics and settler design.

<span id="page-17-1"></span>**1.3.4 Aeration**: Aeration is the process of adding air into wastewater. Providing oxygen for the bacteria that break down organic matter in wastewater is vital, because it acts as the fuel for the aerobic biodegradation of pollutants. Aeration is an essential process in the majority of wastewater treatment plants and accounts for the largest fraction of plant energy costs, ranging from 45 to 75 % of the plant energy expenditure. Aeration systems transfer oxygen into the liquid media by shearing the liquid surface with a mixer or turbine, or by releasing air through macroscopic orifices or porous materials, or through direct contact of air and a large water surface. While analysing or specifying aeration systems, it is important to define efficiency parameters. These are necessary to compare different technologies, as well as to monitor aeration systems over extended time in operation.

## <span id="page-18-1"></span><span id="page-18-0"></span>**CHAPTER 2: OPERATIONAL STATUS OF SEWAGE TREATMENT PLANT IN GANGA FRONT TOWNS (2019)**

#### <span id="page-18-2"></span>**2.1 Monitoring of STPs in Ganga front towns**

Central Pollution Control Board carries out quarterly monitoring of Sewage Treatment Plants and Common Effluent Treatment Plants installed or commissioned or under construction or under trial in Ganga Front Towns under the PIAS project *of Namami Gange* funded by National Mission for Clean Ganga (NMCG). The present study is based on the STP monitoring carried out during June – December, 2019. Monitoring of STPs in Dehradun city of Uttarakhand was also carried out despite the city not being on the bank of river as river Ganga flows through Raiwala area of Dehradun district and hence the treated effluent reaches the river Ganga through river Bindal Rao via river Song.

The inspected STPs were constructed to treat the domestic sewage by adopting technologies such as activated sludge process (ASP), sequencing batch reactor (SBR), up-flow anaerobic sludge blanket (UASB), moving bed biofilm reactor (MBBR) and waste stabilization pond (WSP). Apart from disposing off in river Ganga, a sizeable amount of treated sewage is used for irrigation purposes, gardening etc.

S.No.	<b>Treatment system</b>	<b>Total</b> Number	<b>Total</b> Capacity of STPs (MLD)	Names of STPs& Capacity (MLDs)
1.	<b>Activated Sludge process</b>	19		Uttarakhand (3 nos.) Tehri (5), IDPL (14), Jagjeetpur (18)
	(ASP)			Uttar Pradesh (8 nos.) Narora NAPS (2.2), Jajmau (130), Jajmau (43), Sajari (42), Naini (80), Dinapur (140), Bhagwanpur (9.8), DLW(12)
				Bihar $(2)$ Beur (20), Saidpur (45)
				West Bengal (6) Titagarh (4.5), Naihati (11.56), Bhatpara (10), Bhatpara (8.5), Garden Reach (5.75), Cossipore (45)
2.	Sequencing batch reactor (SBR)	21	325.52	Uttarakhand (17) Gangotri (1), Badrinath (0.26), Joshimath (1.08), Srinagar (1), Sangam Bazar (0.15), Shanti Bazar (0.075), Tapovan (3.5), Swarg Ashram (3), Jagjeetpur (27), Sarai (18), Old Mothrowala (20), New Mothrowala (20), Kargi (68), Jakhan (1), Salawala (0.71), Vijay Colony (0.42), Indira Nagar (5)

<span id="page-18-3"></span>**Table 3: Sewage treatment plants in Ganga front town**





#### <span id="page-20-0"></span>**2.2 Operation & Maintenance of STPs in Ganga states**

#### <span id="page-20-1"></span>**2.2.1 Status of STPs in Ganga front town based on 2019 reports (June – December, 2019)**

Ganga river directly receives treated/untreated sewage from Ganga front towns of five states - Uttarakhand, Uttar Pradesh, Bihar, Jharkhand, and West Bengal. In Ganga front towns, the total sewage generation (2017-18) accounts to approximately 3558.5 MLD. However, the total installed capacity of STPs (December 2019) was 1956.7 MLD and the utilized sewage treatment capacity was1064.2 MLD. There was a gap of 45% in sewage generation and treatment in Ganga front towns. Out of the five states, maximum gap in sewage generation and treatment was found in Bihar (86.5%) followed by West Bengal (65.9%). STPs installed in Bihar were non-operational and no STP was installed in Jharkhand in 2019.



<span id="page-20-2"></span>

Out of the total installed capacity of STPs (1956.7 MLD), 1560.5 MLD was operational and 396.2 MLD was non-operational. Maximum installed capacity was in Uttar Pradesh however no STP was installed in Jharkhand. In Jharkhand, STPs were under trial/construction at Sahibganj town (2 STPs of total capacity 12 MLD) and at Rajmahal town (one STP of capacity 3.5 MLD). The STPs in Patna, Bihar are under upgradation and new STPs are under construction. The non-operational capacity of STPs in West Bengal (288.1 MLD) was higher than the operational capacity (248.1 MLD). In Uttarakhand, 99.95% of the installed capacity was operational.



<span id="page-21-0"></span>**Figure 14: Status of STPs in the five Ganga states w.r.t to treatment capacities.**

During year 2019, a total of 103 STPs were monitored. Out of 103, the highest number of STPs were in Uttarakhand (38) followed by West Bengal (34) and Uttar Pradesh (29). Highest number of non-operational STPs was in West Bengal, where 18 out of 38 STPs were found non-operational.



#### <span id="page-22-0"></span>**Figure 15: Status of STPs in the five Ganga states.**

Based on the characteristics of treated sewage, 70 STPs were complying and 11 were noncomplying with respect to general discharge norms. Six STPs in Uttarakhand and five STPs in Uttar Pradesh were non-complying.

CPCB issued Directions under section 18 (1) (b) of Environment (Protection) Act, 1986 to Uttarakhand Pollution Control Board (UKPCB), Uttar Pradesh Pollution Control Board (UPPCB), Bihar State Pollution Control Board (BSPCB) and West Bengal Pollution Control Board (WBPCB) in June, 2019 to take actions against non-complying, non-operational as well as for STPs without valid consent to operate.



<span id="page-22-1"></span>**Figure 16: Status of STPs in the five Ganga states.**

## <span id="page-23-0"></span>**2.3 Comparative Evaluation of Sewage Treatment Capacity in Ganga Front Towns**

The utilized capacity of all monitored STPs was 42% in 2017-18; which increased to 62% in 2018-19 and reported at 60 % in 2019-20.



<span id="page-23-1"></span>*Figure 17: Comparison of treatment capacities (installed and utilised) in the five Ganga states (2019)* The total number of monitored STPs (doesn't include under construction/under trial STPs) has increased over the years from 68 in 2017-18; 82 in 2018-19; 103 in 2019 December.



<span id="page-23-2"></span>*Figure 18: Graphical representation of increase in number of STPs (2017-18 to 2019-2020)*

#### **CHAPTER 3 FINDINGS AND STATE WISE SPECIFIC OBSERVATIONS**

#### <span id="page-24-2"></span><span id="page-24-1"></span><span id="page-24-0"></span>**3.1. Uttarakhand**

The state wise specific findings on the basis of inspection carried out during December, 2019 are given as below –

- Uttarakhand has 38 STPs which were monitored by CPCB along 15 Ganga front towns. The plants are managed mainly by UK Jal Nigam and UK Jal Sansthan.
- The entire expenses for the operation and maintenance are borne by Government of Uttarakhand.
- The total installed capacity for monitored STPs was 227.71 MLD, with utilized capacity of 137.93 MLD.
- The treated sewage was discharged into River Ganga and its tributaries.
- OCEMS has been installed in 7 STPs out of 38 STPs whereas others are in process of installation of OCEMS.
- The performance of 6 out 38 STPs was found non-complying with respect to discharge standards and 1 STP was found non – operational.
- The STP at Forest Nala (Nandprayag), Old Bridge (Karanprayag), Near SBI Bank (Rudraprayag), Srinagar, 3.5 MLD (Srinagar), Kirtinagar, 0.01 MLD (Kirtinagar) and Kargi (Dehradun) were found non – complying with respect to discharge standards.
- The STP at Ward 1&3, Karanprayag was found non operational on the day of visit due to muddy sewage at the inlet.

#### <span id="page-24-3"></span>**Table 4: Performance of STPs in Uttarakhand**





*All parameters are expressed in mg/l except pH and FC – MPN/100ml*

#### <span id="page-26-0"></span>**3.2 Uttar Pradesh**

The state wise specific findings on the basis of inspection carried out during December, 2019 are given as below –

- 1. Uttar Pradesh has 29 STPs which were monitored by CPCB along 10 Ganga front towns. The plants were managed mainly by UP Jal Nigam.
- 2. The entire expenses for the operation and maintenance are borne by Government of Uttar Pradesh.
- 3. Out of total 29 STPs, 5 were found non- complying with respect to discharge standards and 1 was found non-operational.
- 4. The STPs at Fatehgarh (Farrukhabad), 5 MLD Jajmau STP (Kanpur), Bingawan (Kanpur), Ponghat (Prayagraj) and Kodra (Prayagraj) were found non – complying with respect to discharge standards.
- 5. The STP at Jajmau 43 MLD (Kanpur) was found non operational on day of visit.
- 6. The total installed capacity for monitored STPs was 1133.8 MLD, with utilized capacity of 825.24 MLD.
- 7. The treated sewage is discharged into River Ganga and its tributaries.

<span id="page-26-1"></span>**Table 5: Performance of STPs in Uttar Pradesh**

S.N $\Omega$	<b>STP</b> Name of (Installed	City/Town	Technolog	<b>Utilised</b> Capacity	Analysis result of treated sewage									
	capacity in MLD)		y		pH		<b>BOD</b>		<b>COD</b>		<b>TSS</b>		<b>FC</b>	
					Inlet	Outlet	Inlet	Outlet	Inlet	Outlet	Inlet	Outlet	Inlet	Outlet
General discharge standard			$5.5 - 9.0$ 30			250		$\overline{100}$		1000				
1.	Bijnor (24 MLD)	Bijnor	<b>UASB</b>	12	7.2	7.7	47	8	150	48	75	<b>BDL</b>	$4 \times 10^6$	${}_{5.18}$
2.	Brajghat (3 MLD)	Garhmuktes	<b>UASB</b>	1.5	7.7	7.9	8	5	22	10	82	12		680
3.	Garh (6 MLD)	hwar	<b>SBR</b>	2.69	7.6	7.6	3	$\overline{2}$	13	7	248	<b>BDL</b>		< 18
4.	Fatehgarh (2.7MLD)	Farrukhaba d	<b>WSP</b>	3	8.1	9.4	108	49.7	246	160	245	119	7.9 $\times$ 10 <sup>7</sup>	$3.3 \times$ 10 <sup>5</sup>
5.	Kannauj (13 MLD)	Kannaui	<b>SBR</b>	13	7.6	8.2	18	5.15	60.6	24.6	70.8	27.5		$1.3 \times$ 10 <sup>5</sup>
6.	Jajmau $(43 \text{ MLD})$		ASP	NA	÷,				$\overline{\phantom{a}}$					
7.	Jajmau $(130 \text{ MLD})$		<b>ASP</b>	120	7.3	7.8	150	17.1	461	65.2	455	32	1.6 $\times$ 10 <sup>8</sup>	$2.8 \times$ $10^{7}$
8.	Jajmau $(5 \text{ MLD})$	Kanpur	<b>UASB</b>	$\overline{4}$	7.3	7.4	159	73	370	155	406	38.6	1.6 $\times$ 10 <sup>8</sup>	$1.7 \times$ 10 <sup>7</sup>
9.	(210) Bingawan MLD)		<b>UASB</b>	150	7.6	7.7	119	47.6	269	88.3	412	31.3	5.4 $\times$ 10 <sup>8</sup>	$4.9 \times$ 10 <sup>6</sup>
10.	Sajari (42 MLD)		<b>ASP</b>	15	7.8	8.0	96	12.9	232	27	253	10.8	9.2 $\times$ $10^8\,$	${}_{1.8}$
11.	Salori (29 MLD)	Allahabad	<b>MBBR</b>	11.13	7.3	7.4	37.3	12.6	203	89.8	244	60.3	3.3 $\pmb{\times}$ 106	$1.7\times$ 10 <sup>6</sup>





*All parameters are expressed in mg/l except pH and FC – MPN/100ml*

#### <span id="page-27-0"></span>**3.3 Bihar**

In Bihar, 2 STPs were monitored by CPCB and both were found non – operational.

#### <span id="page-27-2"></span>**Table 6: Performance of STPs in Bihar**

![](_page_27_Picture_930.jpeg)

*All parameters are expressed in mg/l except pH and FC - MPN/100ml* 

#### <span id="page-27-1"></span>**3.4 West Bengal**

The state wise specific findings on the basis of inspection carried out are given as below –

- West Bengal has 34 STPs which were monitored by CPCB along 22 Ganga front towns.
- 18 out 29 STPs were found non operational at time of inspection.
- The reason of high no. of non-operational STPs are: Poorly maintained ponds resulting in Eutrophication, High weed growths, broken walls, floating solid waste etc., de-sludging has not been carried out since long time, no or less sewage was received at inlet due to poor sewerage network or non-functioning of MPS, corroded/damaged equipment of plants, unsatisfactory method of sludge disposal etc.
- The total installed capacity for monitored STPs was 536.17 MLD, with utilized capacity of 101 MLD.

![](_page_28_Picture_544.jpeg)

#### <span id="page-28-0"></span>**Table 7: Performance of STPs in West Bengal**

#### Performance Evaluation STPs in Ganga Front Towns (2019)

![](_page_29_Picture_595.jpeg)

*All parameters are expressed in mg/l except pH and FC – MPN/100ml*

![](_page_30_Picture_285.jpeg)

**Table 8: Status of Sewage Treatment and Utilized Capacity against Sewage Generation from Ganga Front Towns Monitored under PIAS**

#### **Note:**

<span id="page-30-0"></span> No STP was commissioned in Ganga front town of Jharkhand, two STPs were under construction: Sahibganj town (2 STPs total capacity of 12 MLD) and at Rajmahal town (one STP of capacity 3.5 MLD).

No STP was operational in Ganga front town of Bihar during 2019.

The data for sewage generation is approximate and based on data provided by respective SPCBs for the year 2017-18.

Large number of non-functional STPs in West Bengal has proposed plan for upgradation and rehabilitation.

#### **CHAPTER 4 EFFICIENCY OF VARIOUSTREATMENT TECHNOLOGIES**

<span id="page-31-2"></span><span id="page-31-1"></span><span id="page-31-0"></span>**4.1 Activated sludge process (ASP):** The efficiency of the STPs working on ASP technology has been tabulated in the table 8. The following observations can be made from the table:

- 1. The efficiency w.r.t to Biochemical oxygen demand (BOD) was found to range between 66.67%- 100%. The highest efficiency was observed at Tehri STP.
- 2. For COD the STPs running with ASP technology were found to show efficiency between 57%-97.52 % where Tehri STP was found to have highest efficiency
- 3. For TSS the STPs were found to show efficiency between 54.5% 97% where Bhagwanpur STP, Varanasi was found to have highest efficiency at 97% while Cossipore, Chitpur, Bangur STP showed lowest efficiency.

![](_page_31_Picture_346.jpeg)

<span id="page-31-3"></span>**Table 9: Table showing efficiency of STP running with ASP technology**

*Note: In case of outlet value as BDL the efficiency is calculated as 100%*

Performance Evaluation STPs in Ganga Front Towns (2019)

<span id="page-32-0"></span>**4.2 SBR Technology:** The efficiency of the STPs working on the SBR technology has been tabulated in the table9. The following can be inferred from the table:

- 1. Efficiency of the above technology ranges for BOD is found to range between 31%- 99% with highest efficiency of BOD removal at Badrinath STP 0.26 MLD.
- 2. Efficiency of SBR was found to vary between 14%-95% with respect to COD
- 3. With respect to TSS, the efficiency of the STPs ranged between 55% and 98%.

<span id="page-32-2"></span>**Table 10: Table showing reduction efficiency of STP running with SBR technology**

S.	Name of STP		Analysis result of treated sewage				
N <sub>0</sub>	(Installed capacity in MLD)	City/Town	<b>BOD</b> Reduction $(^{0}/_{0})$	<b>COD</b> Reduction $(^{0}/_{0})$	<b>TSS</b> Reduction $(^{0}/_{0})$		
$\mathbf{1}$ .	Gangotri (1 MLD)	Gangotri	93.9	93.8	$\overline{a}$		
2.	Joshimath (1.08 MLD)	Joshimath		14.2	88		
3.	Badrinath (0.26 MLD)	Badrinath	99.5	99.6	$\overline{a}$		
4.	Srinagar (1 MLD)	Srinagar	31.3	22	86.1		
5.	Sangam Bazar (0.075		96.5	94.5	93.4		
6.	Shanti Bazar (0.05	Devprayag	87.2	82.8	86.4		
7.	Tapovan (3.5 MLD)	Tapovan (Rishikesh)	$\frac{1}{2}$	97.5	$\qquad \qquad \blacksquare$		
8.	Swarg Ashram (3 MI.D	Rishikesh	96.7	94.0	$\overline{\phantom{a}}$		
9.	Jagjeetpur (27 MLD)		97.8	83.2	$\frac{1}{2}$		
10.	SaraiJawalapur (14 MLD)	Haridwar	90	93.0			
11.	Mothrowala New(20 MLD)		71.6	68.7	90.1		
12.	Mothrowala Old (20 MLD)		93	92.8	90.5		
13.	Kargi (68 MLD)		95.1	95.5	98.1		
14.	Jakhan (1 MLD)	Dehradun	96.4	94.3	97.7		
15.	Salawala (0.71 MLD)		96.3	95.9	97.6		
16.	Vijay Colony(0.42 MLD)		94.3	92.7	96.1		
17.	Indira Nagar (5 MLD)		92.5	89.4	$\overline{a}$		
18.	Kannauj (13 MLD)	Kannauj	71.4	59.4	61.2		
19.	Salori (14 MLD)	Allahabad		92.0	95.2		
20.	Goithaha (120 MLD)	Varanasi	73.9	58.3	84		
21.	Gayeshpur, Halishar&Kanchrapara $(8.33 \text{ MLD})$	Kanchrapara	82	57.1	55.6		

<span id="page-32-1"></span>**4.3 Waste stabilization pond (WSP):** The efficiency of the STPs working on the WSP technology has been tabulated in the table10. The following observations can be made from the table

- 1. Efficiency of the above technology for BOD was found to range between 53% and 97% with highest efficiency of BOD removal at Anupshahar 1.75 MLD STP.
- 2. Efficiency of WSP was found to vary between 34 % and 92% with respect to COD.
- 3. With respect to TSS, the efficiency of the STPs ranged from 51% to 100%.

<span id="page-33-1"></span>**Table 11: Table showing reduction efficiency of STP running with WSP technology**

	Name of STP (Installed capacity in	City/Town	Analysis result of treated sewage				
S.			<b>BOD</b>	<b>COD</b>	<b>TSS</b>		
N <sub>0</sub>	MLD)		Reduction	Reduction	Reduction		
			$(^{0}/_{0})$	$(^{0}/_{0})$	$(^{0}/_{0})$		
1.	Lakkarghat (6MLD)	Rishikesh	83.9	78.4	88.8		
2.	Fatehgarh (2.7MLD)	Farrukhabad	54 35		51.4		
3.	Vindyachal (4 MLD)	Mirzapur	77.5 75.1		63.7		
4.	<b>Anupsahar STP Zone</b>		$\theta$	$\theta$	81.4		
	A (0.80 MLD)	Anupshahar					
5.	AnupsaharSTP Zone		96.8	92.3	100		
	<b>B</b> (1.75 MLD)						
6.	Titagarh (WSP) (4.5 MLD)	Titagarh	73.6	75.9	87.3		
7.	Bandipur (14 MLD)	Titagarh					
			Non-operational				
8.	Bansberia (0.3 MLD)	Bansberia	Non-operational				
9.	Garulia (4.1 MLD)	Garulia	Non-operational				
10.	Maheshtala (4 MLD)	Maheshtala	Non-operational				
11.	Baidyabati (6 MLD)	Baidyabati	78.6 27.2		31.6		
12.	Kona (30 MLD)	Howrah	Non-operational				
13.	Panihati (12 MLD)	Panihati	Non-operational				
14.	Konnagar (Rishra) (22 <b>MLD</b>	Konnagar	66.7	60	$\overline{17.7}$		
15.	Berhrampore (3.7 MLD)	Murshidabad	Non-operational				
16.	Jiaganj, Azimpur (1.39 <b>MLD</b>	Jiaganj-Azimganj	Non-operational				
17.	Chandannagar	Chandannagar	52.9	52.9	61.8		
18.	Jaggadal - Bhatpara (0.5 <b>MLD</b>	Bhatpara	Non-operational				
19.	Kankinara, Madrail (10	Bhatpara	Non-operational				
20.	<b>MLD</b> Hatisur (10 MLD)	Kolkata	63.7	50	13.8		
21.	Nabadwip (10.5 MLD)	Nabadwip	58.38	59.9	61.2		
22.	Kalyani Town area (10 MLD)	Kalyani	94.6	70.3	94.6		

*Note: In case of outlet value as BDL the efficiency is calculated as 100%*

<span id="page-33-0"></span>**4.4 Up flow anaerobic sludge blanket (UASB):** The efficiency of the STPs working on the UASB technology has been tabulated in the table11. Following observations can be made from the table:

- 1. Efficiency of the above technology for BOD was found to range between 33% 83%.
- 2. Efficiency of UASB was found to vary between 46%- 75 % with respect to COD.

3. With respect to TSS, the efficiency of the STPs ranged between 85.36 % and 92%.

	Name of STP		Analysis result of treated sewage				
S.	(Installed capacity in MLD)	City/Town	<b>BOD</b>	<b>COD</b>	<b>TSS</b>		
No			Reduction	Reduction	Reduction		
			$\binom{0}{0}$	$($ %)	$\binom{0}{0}$		
1.	Bijnor (24 MLD)	Bijnor	83	68			
2.	Brajghat (3 MLD)	Garhmukteshwar	37.5	54.5	85.4		
3.	Garh (6 MLD)		33.3	46.2			
4.	Jajmau (5 MLD)		54.1	58.1	90.5		
5.	Bingawan (210 MLD)	Kanpur	60	67.2	92.4		
6.	Rajapur (60 MLD)	Allahabad	64.2	61.9	92		
7.	PakkaPokhra (14 <b>MLD</b>	Mirzapur	81.3	74.9	89.5		

<span id="page-34-2"></span>**Table 12: Table showing reduction efficiency of STP running with UASB technology**

<span id="page-34-0"></span>**4.5 Moving Bed Biofilm reactor (MBBR):** The efficiency of the STPs working on MBBR technology has been tabulated in the table12. The following observations can be made from the table

- 1. Efficiency of the above technology ranges for BOD was found to range between 66 % and 94%.
- 2. Efficiency of MBBR system was found to vary between 55 % and 93 % with respect to COD.
- 3. With respect to TSS, the efficiency of the STPs ranged from 41% to 100%.

<span id="page-34-3"></span>**Table 13: Table showing reduction efficiency of STP running with MBBR technology**

![](_page_34_Picture_383.jpeg)

*Note: In case of outlet value as BDL the efficiency is calculated as 100%*

<span id="page-34-1"></span>**4.6 Electro-coagulation (EC):** The efficiency of the STPs working on the EC technology has been tabulated in the table 13. Following observations can be made from the table

1. Efficiency of the above technology ranges for BOD is found to range between 43% and 90 %

- 2. Efficiency for COD reduction was found to vary between 48 % and 94 %
- 3. With respect to TSS, the efficiency of the STPs ranged from 46% to 96%.

#### <span id="page-35-0"></span>**Table 14: Table showing reduction efficiency of STP running with Electro-coagulation technology**

![](_page_35_Picture_494.jpeg)

#### <span id="page-35-1"></span>**Table 15: Table showing reduction efficiency of STP running with other technology**

![](_page_35_Picture_495.jpeg)

## **CHAPTER 5 CONCLUSION**

<span id="page-36-1"></span><span id="page-36-0"></span>The study was done to assess the performance evaluation and compliance verification of sewage treatment plants installed in Ganga front towns. There are various technologies in use for the treatment of raw sewage before their discharge into surface water system viz. biological treatment and non-biological systems. The biological treatment systems use either the aerobic, anaerobic or facultative digestion method to degrade the organic content present in the raw sewage followed by tertiary treatment at many plants and ultimately discharges the treated sewage after disinfection to control the number of pathogenic organism within limits. However, non-biological treatment system such as electrocoagulation technology based system is also installed at some towns which use electrochemical technology followed by tertiary treatment and ozone based disinfection system. During the present study, analysis of different treatment technologies was carried out for their treatment efficiency. Some of the important conclusory remarks are as follows

- -
- The utilized capacity of all monitored STPs has increased over past three years, which was 42% in 2017-18; and increased to 62% in 2018-19 and reported as 60 % in 2019-20. The total number of monitored STPs has increased over the years from 68 in 2017-18; 82 in 2018-19 and 103 in 2019-20.
- In state of Uttarakhand, 31 out of 38 STPs were found complying with respect to discharge standards and 1 STP was found non – operational. In Uttar Pradesh, 24 out of 29 STPs were found complying with respect to discharge standards. Both STPs of Bihar were found to be non-operational at the time of inspection. 18 out of29 STPs of West Bengal were found to be non – operational at the time of inspection.
- In Bihar and West Bengal, most of the STPs were either under-construction/ upgradation under the *Namami Gange* Programme. Recently, 2 STP in Bihar with a total of 80 MLD capacity (43 MLD Beur STP and 37 MLD Karmalichak STP) were made operational.
- The efficiency of SBR technology was found to be higher than other technologies in terms of removal of organic pollutants from raw sewage. Though ASP and OP

technologies have shown slightly lower efficiency than that of SBR technology, have promising efficiency to reduce the pollution load of raw sewage, the main objective of sewage treatment.

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